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In the claims:

Please amend the claims as shown below:

- 5 1. (Currently amended) A method for continuous alkali oxygen
delignification of digested cellulose pulp and of cellulose
pulp that has been washed after digestion, comprising:
10 ~~which storing pulp is stored in a storage tower or pulp
chute at essentially atmospheric pressure, and that~~
maintainings a medium consistency of the pulp in a the range
of 8-18%, and that maintainings the cellulose pulp to be
delignified at a kappa value of at least 15 units,
15 ~~preferably a kappa exceeding 20 units, where the oxygen
delignification takingtakes place in a reactor system with~~
several oxygen reactors with a predetermined retention time
of the cellulose pulp in the reactor system, where adding
alkali is added to the cellulose pulp in order to obtain an
initial pH exceeding 9.0 and addingwhere oxygen is added to
20 the cellulose pulp at an amount of 5-50 kg per tonne of
pulp at a position before a first oxygen reactor in the
reactor system, providingand where the pulp withhas a
predetermined total retention time of greater than 45
minutes in the reactor system, characterised in
that, in association with anthe addition of the necessary
25 chemicals chemicals and an initial mixing-in operation,
placing the cellulose pulp is placed under pressure at an
initial pressure of greater than 15.0 bar, subjectingafter
which the pulp is subject to more than one remixing
position where a the final pressure after a the final
30 remixing position is at least 13 bar, subjecting the pulp
toand with a minimum retention time in a highin this first
high pressure section of at least 3-10 minutes,
reducingafter which the pressure of the pulp is reduced to
a pressure that lies under 10-12 bar, heating the pulp with

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~~and is heated by steam such that at the~~ temperature of the
pulp is raised by at least 5 °C by the addition of steam,
~~and leading followed by the heated pulp being led to a~~
reactor system in a low pressure section with a retention
time that exceeds the retention time in the ~~high~~ pressure
section.

2. (Currently amended) The method according to claim 1,
~~characterised in that wherein~~ oxygen, preferably the
major part of the oxygen added for the oxygen stage, is
added to the cellulose pulp immediately after the initial
pressure of more than 15 bar has been established.

3. (Currently amended) The method according to claim 2,
~~characterised in that wherein~~ the remixing positions
are constituted by fluidising mixers, either in ~~at the~~ form
of a fluidising pump, a fluidising restriction, a
fluidising mixer or a restriction in ~~at the~~ flow that results
in a fall in pressure of less than 1 bar.

4. (Currently amended) The method according to claim 3,
~~characterised in that wherein~~ a first high pressure
reactor is located after the initial mixing-in operation,
in which reactor the cellulose pulp is given a first
retention time of t_1 , and in that a high pressure reactor
follows after the remixing positions in the high pressure
section after each one of the remixing positions.

5. (Currently amended) The method according to claim 4,
~~characterised in that wherein~~ the reactors in the
high pressure section are dimensioned such that the
cellulose pulp is given successively longer retention
times, such that ~~when~~ the number of reactors is X, the
retention times are $t_1 - t_x$ for each relevant reactor $R_1 -$
 R_x , where $t_1 < t_2 < \dots < t_x$.

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6. (Currently amended) The method according to claim 5,
~~characterised in that~~wherein the retention times t_1
- t_x in the reactors R_1 - R_x in the high pressure section
5 are expressed as
 $t_{\min} = 1$ minute for t_1 , after which ($t_x = 2 * t_{x-1}$) and $T_{\max} =$
 $X * 10$ minutes;
 $(t_1 = 1-10 \text{ min.}, t_2 = 2-20 \text{ min.}; t_3 = 4-30$
 $\text{min.}; t_4 = 8-40 \text{ min. etc.}),$
10 where $t_x < t_{x+1}$.
7. (Currently amended) The method according to ~~any one of the~~
~~preceding claims, characterised in that~~ claim 1
15 wherein a stirrer is present in at least one high pressure
reactor, which stirrer acts in at the principal part ~~(greater~~
~~than 50%)~~ of at the reactor volume, either in at the form of a
mechanical stirrer (S) or hydrodynamic stirrers that at
least circulate free fluid in the reactor.
- 20 8. (Currently amended) The method according to ~~any one of the~~
~~preceding claims, characterised in that~~ claim 1
wherein at least one of the oxygen and and alkali additions
are ~~can be~~ added to the cellulose pulp in association with
the remixing positions in the high pressure section at an
25 amount that is lower than the amount that is added at the
initial mixing-in operation, and ~~in that~~ at least one of
the oxygen and alkali additions are ~~can be~~ added batch-wise
at at the beginning of the low pressure section.
- 30 9. (Currently amended) The method according to ~~any one of the~~
~~preceding claims, characterised in that~~ claim 1
wherein the cellulose pulp is dewatered before the oxygen
delignification to a higher consistency and ~~in that it the~~
cellulose pulp is re-diluted before the oxygen
35 delignification to a medium consistency with pure filtrate

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that has preferably been previously oxidized, and in that
alkali in athe form of oxidized white liquor is used in
the oxygen delignification.